## Capturing CO2 from Biogas by MEA (Monoethanolamine) using Packed Bed Scrubber

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### Capturing CO<sub>2</sub> from Biogas by MEA (Monoethanolamine) using Packed Bed Scrubber

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#### ABSTRAK

Biogas adalah salah satu sumber energi terbarukan yang dapat dimanfaatkan sebagai pengganti energi fosil. Biogas sebagian besar mengandung metan (CH<sub>4</sub>) dan karbon dioksida (CO<sub>2</sub>). Kandungan CO<sub>2</sub> pada biogas mengurangi efisiensi pada proses pembakaran dan dapat menyebabkan korosi pada komponen-komponen logam yang kontak langsung dengan biogas. Pemurnian biogas dengan absorpsi merupakan suatu cara untuk menurunkan kadar CO<sub>2</sub> yang terkandung, dan meningkatkan kandungan CH<sub>4</sub> pada biogas sehingga biogas yang dihasilkan dapat digunakan sebagai bahan bakar. Penelitian ini ditujukkan untuk mempelajari pengaruh konsentrasi monoethanolamine (MEA) dan laju alir absorben terhadap penurunan kadar CO<sub>2</sub> yang terkandung dalam biogas. Proses absorpsi CO<sub>2</sub> dilakukan pada scrubber tipe *spray tower*, *scrubber* yang digunakan pada penelitian ini berbahan akrilik dengan diameter 64 mm, panjang *scrubber* 750 mm, tinggi packing pada *scrubber* 500 mm dan dengan kapasitas 1.5 m<sup>3</sup>. Laju alir biogas yang digunakan 26 L/menit dengan variasi laju alir larutan MEA sebesar 0,5, 1 dan 1,5 L/menit dan variasi konsentrasi larutan MEA sebesar 1, 3, 5, dan 7M. Hasil penelitian menunjukkan pada laju alir larutan MEA 1,5 L/menit dengan konsentrasi larutan MEA 7M dapat menurunkan CO<sub>2</sub> dari 8,53% menjadi 0,10%, dan dapat meningkatkan kandungan metana (CH<sub>4</sub>) dari 69,24% menjadi 81,20%.

Kata kunci: absorpsi; biogas; MEA; packed bed scrubber; pemurnian biogas

#### ABSTRACT

Biogas is a renewable energy source that can be used as a substitute for fossil energy. Biogas mostly contains methane (CH<sub>4</sub>) and carbon dioxide (CO<sub>2</sub>). The content CO<sub>2</sub> in biogas reduces the efficiency of the combustion process and cause corrosion in metal components when direct contact with biogas. Biogas purification using absorption method can reduce levels of CO<sub>2</sub> contained and increase levels of CH<sub>4</sub> then the biogas produced can be used as fuel. This research study the effect of monoethanolamine (MEA) concentration and absorbent flow rate on the reduction of CO<sub>2</sub> contained in biogas. CO<sub>2</sub> absorption process is carried out by a spray tower type scrubber. It consisted of an acrylic absorption column (64 mm in diameter, 750 mm in height, 500 mm in packing height and 1.5 m<sup>3</sup> in capacity). Biogas flow rate used is 26 L/min with variation of the flow rate of MEA 0.5, 1, and 1,5 L/min and concentration of 7M MEA solution 1, 3, 5, and 7M. The results showed that the flow rate of MEA 1.5 L/min with a concentration of 7M MEA solution can reduce CO<sub>2</sub> from 8.53% to 0.10% and can increase the methane (CH<sub>4</sub>) load from 69.24% to 81.20%.

Keywords: absorption; biogas; biogas purification; MEA; packed bed scrubber

#### 1. INTRODUCTION

Fossil energy consumption in Indonesia is increasing every year. Energy reserves are running low, it is feared that fossil energy sources in Indonesia will soon run out (there needs to be an effort to overcome the energy scarcity that will be faced by Indonesia). Therefore, to overcome the problem of global energy needs that continue to increase, efforts are needed to utilize alternative sources, namely through efforts to utilize agricultural, plantation or forest product residues and household organic waste in the form of biomass. Today biomass has become the

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most popular energy source in every region of the world [1]. Biomass has great potential to become one of the alternative energy sources in the future [2]. Biomass energy sources have very potential in Indonesia, including biodiesel and biogas. Biodiesel is an alternative fuel sourced from plants and animal fats, Crude Palm Oil (CPO), waste cooking oil, and algae plants, while it is predicted that biodiesel consumption in Indonesia in 2025 will increase to 6.9 million kiloliters [3-6]

Biogas is one of a variety of new renewable energy that is continuously being developed at this time. Biogas is a mixture of flammable gases that comes from the anaerobic digestion process. Compounds contained in biogas include  $CH_4$ ,  $CO_2$  and other compounds in small amounts [7]. The biogas produced can be directly used as fuel for biogas stoves, but biogas without purification is still high in  $CO_2$  content, it needs to be purified in the biogas produced to be used as fuel.

Biogas which is formed from the organic waste fermentation process does not have a gas content that is 100% flammable. Biogas products consist of CH<sub>4</sub> 55-65%, CO<sub>2</sub> 35-45%, nitrogen (N<sub>2</sub>) 0-0.3%, hydrogen (H<sub>2</sub>) 1-5%, H<sub>2</sub>S 0-3%, oxygen (O<sub>2</sub>) 0.1-0.5%, and water vapor. all of these elements that play a role in determining the quality of biogas namely methane and carbon dioxide [8-9].

To increase the utilization of biogas as renewable energy, it is necessary to carry out the stages of refining methane. Biogas purification techniques can be carried out by the absorption method, which is the separation of a particular gas from a mixture of gases by transferring mass into a liquid that has a different solvent selectivity from the gas to be separated. Various kinds of biogas purification methods include physical absorption, chemical absorption, absorption separation with membranes, cyrogenic and chemical conversion into other compounds [10]. There is also to capture  $\bigcirc D_2$  with solvents various such as ammonia, tetrahydrofuran, monoethanolamine and

#### tetra-n-butyl ammonium bromide [11-12].

The purity of  $CO_2$  and  $H_2S$  content in biogas is very important for the machine because it affects the heating value and the life of the device that uses biogas. Carbon dioxide is an inhibitor of the rate of combustion chemical reactions in the engine [13].  $CO_2$  compounds reduce the heating value of combustion, it is necessary to eliminate or reduce this  $CO_2$ content. Pure CH<sub>4</sub> has a calorific value of 9100 kcal/m<sup>3</sup> at 15.5°C and 1 atmosphere, while the caloric value of biogas combustion is around 4800–6900 Kcal/m<sup>3</sup> [14].

In the biogas production process, the biogas products produced contain H<sub>2</sub>S ranging from 100-10000 ppm, the H<sub>2</sub>S content depends on the type of biomass and organic material it contains [15]. H<sub>2</sub>S has been identified as a compound that causes corrosion in machining components. Using biogas that contains H<sub>2</sub>S will produces sulphur and sulfuric acid which are corrosive to various types of metals. H<sub>2</sub>S content of 200 ppm if inhaled by humans for 30 minutes can cause death. The maximum permit for H<sub>2</sub>S for safety and health standards is 20 ppm [16]. When H<sub>2</sub>S contained in biogas burns, H<sub>2</sub>S will turn into sulfur oxides (SO<sub>X</sub>) which will cause corrosion on metal components and make engine lubricating oils acidic. To reduce the damage caused by H<sub>2</sub>S, the H<sub>2</sub>S compound must be removed or reduced to the tolerance level [17].

Various methods for removing CO2 and H2S content such as physical adsorption, catalyst conversion [18]. Between NaOH solution, ethylene glycol, MEA and DEA, MEA solution has the highest efficiency in the absorption of CO<sub>2</sub> and H<sub>2</sub>S [19]. Amine solution which is used as an absorber of CO<sub>2</sub> and H<sub>2</sub>S in biogas in the scrubber, has a very high selectivity in terms of absorption of CO<sub>2</sub> and  $H_2S$  [20]. MEA is an amine solution that is best used as an absorption process, this is because MEA has the highest ability to absorb CO<sub>2</sub> compared to diethanolamine (DEA) and methyl diethanolamine (MDEA) [21]. The concentration of MEA as a solution to bind CO<sub>2</sub> needs to be considered because it can improve the quality of purified biogas [22-24].

The design of a packed bed scrubber is very important. The size column and packing size affect the process of purification. Previous researchers have done various modifications to the size of the purification column by using MEA solution as an absorber. Scrubber with a diameter of 70 mm, height of 1000 mm with the the rasch ring, using 1M MEA solution. The result of this study CO<sub>2</sub> removal efficiency reaches 73% [23]. Furthermore, scrubber size 600 mm in height and 30 mm in diameter with the the rasch ring packing. The result of this study CO<sub>2</sub> removal efficiency reaches 65% [22].

Next research with size column 780 mm in height and 120 mm in diameter using MEA solution as an absorber increased the CH<sub>4</sub> content from 70% to 92% and decreased the CO<sub>2</sub> content from 30% to 5% in the biogas by purification [25].

In this tudy the the packed bed scrubber is made of an acrylic absorption column (64 mm in diameter, 750 mm in height, 500 mm in packing height and 1.5m<sup>3</sup> in capacity).

#### 2. METHODS

In this study began with a literature study on the process of making biogas and the process of purification of biogas, then the preparation of materials for the manufacture of packed bed scrubbers, during the process of making tools, made biogas with raw materials cow dung and water 1: 2. The making of biogas uses a fixed dome type biodigester with a capacity of 500 liters found in the State Polytechnic of Sriwijaya Laboratory.

Biogas purification process requires a tool to reduce  $CO_2$  content, various methods and tools used in biogas purification, one of which is by using a packed bed scrubber tool. Figure 1 is a picture of a packed bed scrubber tool used in this study, this tool is equipped with a temperature sensor to see the temperature changes that occur during the purification process, and is equipped with a biogas pump that functions so that the gas flow rate that enters during the purification process is constant.

This unit have dimension: 416 x450 x 1.170 mm, with scrubber diameter 64 mm and length 500 mm, in the scrubber have rasch ring packing with dimension 10 mm in height, 5 mm in diameter. This unit equipped with biogas pump (flow rate 26 L/min) and solution pump.

Biogas produced from fixed dome type biodigesters, biogas was analyzed for the composition of biogas at 5-day intervals, on days 5, 10, 15, 20, 25, and 30, then purification was carried out on the biogas produced using monoethanolamine.

In this research used MEA of loba chemie brand with 99% concentration. The process of purification  $CO_2$  by varying the concentration of MEA (1M, 3M, 5M, 7M) and varying the flow rate (0.5 L/min 1 L/min and 1.5 L/min). The biogas from digester collect using 30 L biogas bag, after that the biogas in 30 L is purified then stored in 2 L biogas bag.

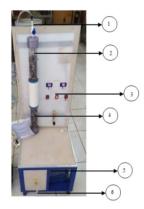
Biogas analysis was carried out in the PT Pupuk Sriwijaya Palembang laboratory using Shimadzu GC-2014 gas chromatograph. The Shimadzu GC-2014 is a highly versatile gas chromatograph system. The GC unit is ideal for both routine analysis like in chemicals analysis. Biogas in sample bag injected into the Shimadzu GC-2014, the result of data analysis from this GC is using concentration of the biogas.

#### 3. RESULTS AND DISCUSSION

Biogas production is carried out at a biogas installation in the State Polytechnic of Sriwijaya (Renewable Energy Laboratory), the digester used can be seen in Figure 1 and the packed bed scrubber used in this study can be seen in Figure 2.



Figure 1. fixed dome Biodigester [26]



**Figure 2.** Packed bed scrubber. (1) Biogas output, (2) Scruber, (3) Control panel, (4) Packing, (5) Solution tank, (6). Biogas input.

The biogas produced is stored in a 30 L bag, then the biogas is connected to the biogas input to the absorber for absorption by the output of a 2 L biogas sample bag. The biogas purification results used MEA solution before and after purification on packed bed scrubber in Table 1 and Table 2.

## 3.1 ANALYSIS RESULT BEFORE AND AFTER PURIFICATION

Observation data were obtained by analyzing biogas samples at PT Pupuk Sriwijaya Palembang. The purpose of the analysis is to determine the content of CH<sub>4</sub>, CO<sub>2</sub>, O<sub>2</sub> and N<sub>2</sub> contained in biogas. Following are the results of the analysis of biogas composition before being purified.

Biogas analysis before purification is conducted at intervals of 5 days, the point is to find out the optimum biogas content condition. On the  $5^{\text{th}}$  day the digester did not produce biogas, entering the  $10^{\text{th}}$  day the biogas was formed but the methane content was still low. Result data analysis biogas composition before purification 5 days interval in Table 1.

Entering the  $15^{th}$  day the composition began to increase CH<sub>4</sub> 44.42%, CO<sub>2</sub> 1.64%, O<sub>2</sub> 16.96% and N<sub>2</sub> 35.28%.

Table 1. Biogas composition before	purification from biodigester	production in 5-30 days
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Biodigester production time (days)	Biogas Composition (%)			
	CH <sub>4</sub>	$CO_2$	$O_2$	N <sub>2</sub>
5	0	0	0	0
10	19.18	0.93	19.54	58.80
15	44.42	1.64	16.96	35.28
20	60.27	3.05	14.27	20.61
25	71.18	8.53	6.65	12.28
30	62.04	14.64	3.27	18.28

On the 20<sup>th</sup> day and the 25<sup>th</sup> day the CH<sub>4</sub> content continued to increase with an optimal composition on the 25<sup>th</sup> day showing that the CH<sub>4</sub> content reached 71.18%, CO<sub>2</sub> 8.53% O<sub>2</sub> content decreased to 6.65% and N<sub>2</sub> also decreased to 12.28%.

Day 30 there was a decrease in biogas production, the results of biogas composition

analysis on day 30 decreased compared to day 25th CH<sub>4</sub> 62.04%, CO<sub>2</sub> 14.64%, O<sub>2</sub> 3.27% and N<sub>2</sub> 18.28%. Therefore, researchers purified using biogas which was produced on the 25<sup>th</sup> day as a gas for the purification process, because the optimum methane content was found on the 25<sup>th</sup> day, 71.18% with CO<sub>2</sub> content of 8.53%.

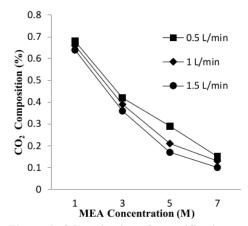
Purification process is to reduce CO<sub>2</sub> content in biogas, decreasing CO<sub>2</sub> content in biogas, the methane content will increase. Data from analysis of biogas content after purification in Table 2.

MEA Flow Rate	MEA	Biogas Composition (%)			
(L/min)	Concentration (M)	CH4	CO <sub>2</sub>	O2	N <sub>2</sub>
0.5		72.64	0.68	7.65	17.10
1	1	73.52	0.66	7.36	16.56
1.5		73.74	0.64	7.52	16.13
0.5		75.77	0.42	6.52	15.42
1	3	76.04	0.39	6.77	15.37
1.5		76.23	0.36	6.53	15.28
0.5		77.30	0.29	6.57	14.20
1	5	77.41	0.21	6.34	14.53
1.5		78.04	0.17	6.80	13.54
0.5		79.07	0.15	6.80	11.55
1	7	80.24	0.13	6.41	11.78
1.5		81.20	0.10	6.89	11.01
				1	

Table 2. Biogas composition after purification by MEA using packed bed scrubber

### 3.2 ANALYSIS RESULT CO<sub>2</sub> AND CH<sub>4</sub> AFTER PURIFICATION

Figure 3 is dath that has been processed into a graph of the effect of flow rate and concentration of MEA to  $CO_2$  reduction after purification.



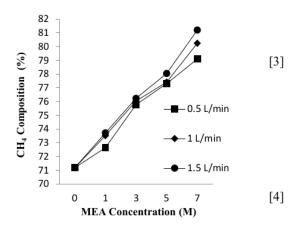
**Figure 3.** CO<sub>2</sub> reduction after purification using MEA at flow rate of 0.5, 1, 1.5 L/min

The results of biogas analysis after purification showed very significant results at

a MEA flow rate of 0.5 L/min with a concentration of 1M MEA able to reduce CO<sub>2</sub> from 8.53% to 0.68% (Figure 3). Increasing the flow rate and concentration of MEA makes the CO<sub>2</sub> content decreases. This is due to the greater absorbent flow rate that will make an increase in the interfacial area of packing in the column. This is in line with research conducted by W. Kamopas et al. [25] which examined the effect of flow rate and concentration of MEA on gas purification. From his research proved that the rate of solution and the higher concentration of MEA that enters the scrubber can reduce CO<sub>2</sub>. Furthermore, along with a decrease in  $CO_2$  content in by gas, an increase in CH<sub>4</sub> content in biogas, the effect of the flow rate and the concentration of MEA on CH<sub>4</sub> can be seen in Figure 4.

In Figure 4, increasing the flow rate and the concentration of MEA make  $CH_4$  contend inscrease. Concentration in biogas has increased from 71.18 to 81.20%.  $CH_4$  has one carbon in each chain can produce more environmentally friendly combustion than long carbon chain fuels. This is due to the amount of  $CO_2$  produced during the

combustion of short or fewer carbon chain fuels.



**Figure 4.** Effect of the MEA solution flow rate of 0.5, 1, 1.5 L/min on CH<sub>4</sub>

#### 4. CONCLUSIONS

The results of the study using MEA solution [5] with Packed Bed Scrubber showed that the higher the flow rate of the solution and the higher the concentration of the solution would increase the absorption of CO2 and increase the CH<sub>4</sub> content. The optimum results obtained at a solution flow rate of 1.5 L/min with a 7 M MEA concentration obtained a decrease in CO2 content from 8.53% to 0.1%, while the CH<sub>4</sub> content from [6] 71.18% to 81.20%, in this study obtained the best percentage reduction in CO2 8.52% and in CH<sub>4</sub> increase 10.02%. The parameters carried out in this study are expected to be a reference for optimizing biogas purification.

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